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# EE C245 - ME C218 Introduction to MEMS Design Fall 2011

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Lecture Module 3: Oxidation & Film Deposition

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## Lecture Outline

- Reading: Senturia, Chpt. 3; Jaeger, Chpt. 2, 3, 6
  - ↳ Example MEMS fabrication processes
  - ↳ Oxidation
  - ↳ Film Deposition
    - Evaporation
    - Sputter deposition
    - Chemical vapor deposition (CVD)
    - Plasma enhanced chemical vapor deposition (PECVD)
    - Epitaxy
    - Atomic layer deposition (ALD)
    - Electroplating

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## MEMS Fabrication

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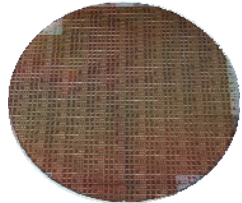
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## Making Mechanical Devices

- How best does one make a mechanical product?
- Assembly line production?
  - ↳ Pick and place parts
  - ↳ Used for many macroscopic mechanical products
  - ↳ Robotic automation greatly reduces cost
- **Problem:** difficult to do this with MEMS-scale parts (but not impossible, as we'll soon see ...)
- **Solution:** borrow from integrated circuit (IC) transistor technology
  - ↳ Use monolithic wafer-level fabrication methods
  - ↳ Harness IC's batch methods, where multiple devices are achieved all at once



Automobile Assembly Line



CMOS Integrated Circuit Wafer

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### Polysilicon Surface-Micromachining

- Uses IC fabrication instrumentation exclusively
- **Variations:** sacrificial layer thickness, fine- vs. large-grained polysilicon, *in situ* vs. POCL<sub>3</sub>-doping

300 kHz Folded-Beam Micromechanical Resonator

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### Electroplating: Metal MEMS

- Use electroplating to obtain metal structures
- When thick: call it "LIGA"
- **Pros:** fast low temp deposition, very conductive
- **Cons:** drift, low mech. Q but may be solvable?

RF Switch

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### Bulk Micromachining and Bonding

- Use the wafer itself as the structural material
- **Adv:** very large aspect ratios, thick structures
- **Example:** deep etching and wafer bonding

Micromechanical Vibrating Ring Gyroscope

[Najafi, Michigan]

Microrotor (for a microengine)

[Pisano, UC Berkeley]

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### Oxidation

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### Thermal Oxidation of Silicon

- Achieved by heating the silicon wafer to a high temperature (~900°C to 1200°C) in an atmosphere containing pure oxygen or water vapor
- Enabling reactions:
  - For dry oxygen:  $\text{Si} + \text{O}_2 \rightarrow \text{SiO}_2$
  - For water vapor:  $\text{Si} + 2\text{H}_2\text{O} \rightarrow \text{SiO}_2 + 2\text{H}_2$

**Schematically:**

High T (~900°C - 1200°C)  
In dry O<sub>2</sub> or Water vapor

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### Oxidation Modeling

(1) **Initially:** (no oxide @ surface)

↳ Growth rate determined by reaction rate @ the surface

(2) **As oxide builds up:**

↳ Growth rate governed more by rate of diffusion to the silicon-oxide interface

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### Oxidation Modeling (cont.)

**reactant concentration**

$N_0$  = reactant conc. at oxide surface [in cm<sup>-2</sup>]  
 $N_i$  = reactant conc. at Si-SiO<sub>2</sub> interface

$J$  = reactant flux =  $-D \frac{\partial N(x,t)}{\partial x}$  [Fick's 1<sup>st</sup> Law of Diffusion]  
 Diffusion coeff. [in μm/hr or m/s]

**distance from surface**

surface    Si-SiO<sub>2</sub> interface

**In the SiO<sub>2</sub>:**  $J = D \frac{(N_0 - N_i)}{X_{ox}} = \text{constant}$  (1)  
 [in # particles/(cm<sup>2</sup>·s)]    Assumption that the reactant does not accumulate in the oxide.

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### Oxidation Modeling (cont.)

**At the Si-SiO<sub>2</sub> interface:**  
 Oxidation rate  $\propto N_i \therefore J \propto N_i \Rightarrow J = k_s N_i$  (2)  
 Reaction rate constant @ Si-SiO<sub>2</sub> interface

**Combining (1) and (2):**

$$\left[ N_i = \frac{J}{k_s} \right] \Rightarrow J = D \left( \frac{N_0 - J/k_s}{X_{ox}} \right)$$

$$J X_{ox} = D N_0 - \frac{D J}{k_s} \rightarrow J \left( X_{ox} + \frac{D}{k_s} \right) = D N_0$$

$\therefore J = \frac{D N_0}{X_{ox} + \frac{D}{k_s}} = \text{Flux of reactants}$

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### Oxidation Modeling (cont.)

Find an expression for  $X_{OX}(t)$ :

oxidizing flux

$$\left. \begin{array}{l} \text{Rate of change of oxide} \\ \text{layer thickness w/time} \end{array} \right\} = \frac{dX_{OX}}{dt} = \frac{J}{M} = \frac{DN_{O_2}/M}{X_{OX} + D/k_s} \quad (3)$$

# of molecules of oxidizing species incorporated into a unit volume of oxide

$$\left. \begin{array}{l} = 2.2 \times 10^{22} \text{ cm}^{-3} \text{ for } O_2 \\ = 4.4 \times 10^{22} \text{ cm}^{-3} \text{ for } H_2O \end{array} \right\}$$

Solve (3) for  $X_{OX}(t)$ : [Initial condition  $X_{OX}(t=0) = X_i$ ]

$$\frac{dX_{OX}}{dt} = \frac{DN_{O_2}/M}{X_{OX} + D/k_s} \Rightarrow \int_{X_i}^{X_{OX}} \left( X_{OX} + \frac{D}{k_s} \right) dX_{OX} = \int_0^t \frac{DN_{O_2}}{M} dt$$

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### Oxide Thickness Versus Time

**Result:**

additional time required to go from  $X_i \rightarrow X_{OX}$       time required to grow  $X_i$  [ $X_i$  = initial oxide thickness]

$$X_{OX}(t) = \frac{A}{2} \left\{ \left[ 1 + \frac{4B}{A^2} (t + \tau) \right]^{1/2} - 1 \right\}$$

where  $A = \frac{2D}{k_s}$        $\tau = \frac{X_i^2}{B} + \frac{X_i}{(B/A)}$

$$B = \frac{2DN_{O_2}}{M} \quad D = D_0 \exp\left(-\frac{E_A}{kT}\right)$$

[ i.e., D governed by an Arrhenius relationship  $\rightarrow$  temperature dependent ]

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### Oxidation Modeling (cont.)

**For shorter times:**

$$\left[ (t + \tau) \ll \frac{A^2}{4B} \right] \Rightarrow X_{OX}(t) = \left( \frac{B}{A} \right) (t + \tau) \Rightarrow$$

oxide growth limited by reaction at the Si-SiO<sub>2</sub> interface

Taylor expansion (first term after 1's cancel)      linear growth rate constant

**For long oxidation times: oxide growth diffusion-limited**

$$\left[ (t + \tau) \gg \frac{A^2}{4B} \right] \Rightarrow X_{OX}(t) = \sqrt{B(t + \tau)} \approx \sqrt{Bt}$$

$t \gg \tau$       Parabolic rate constant

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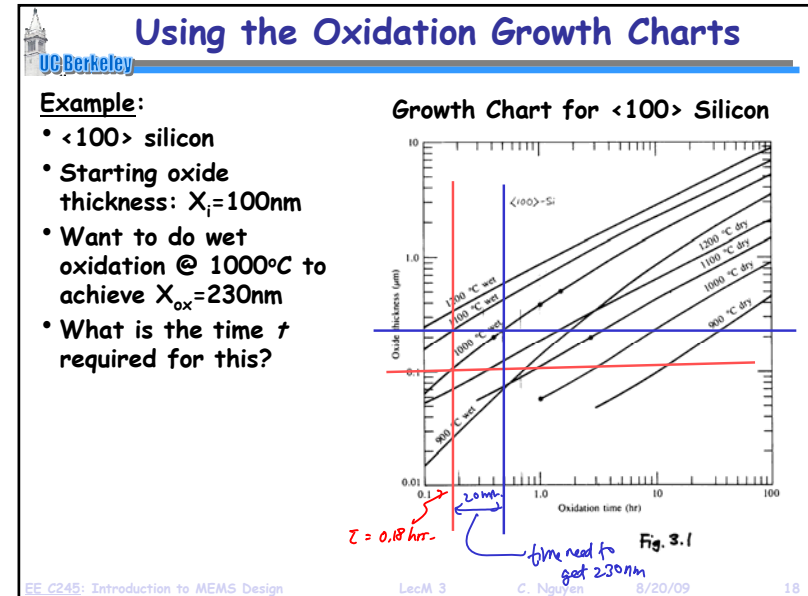
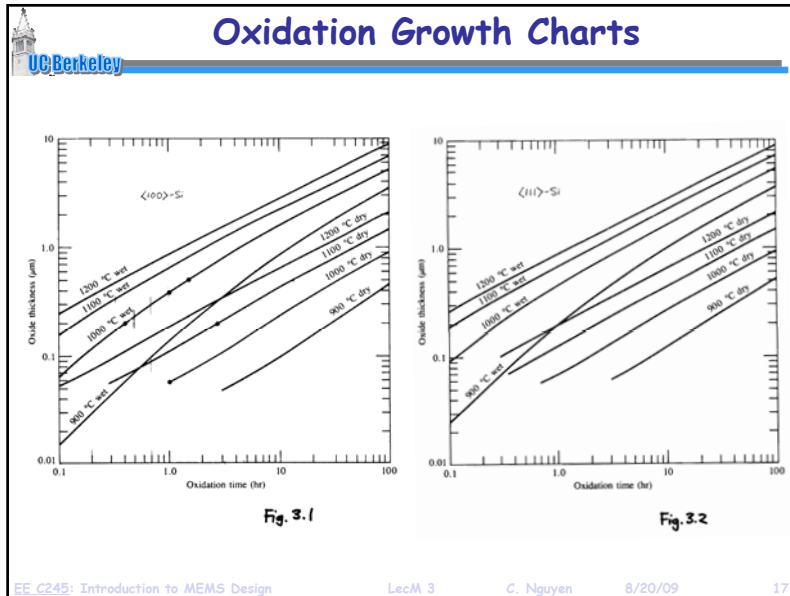
### Oxidation Rate Constants

**Table 6-2** Rate constants describing (111) silicon oxidation kinetics at 1 Atm total pressure. For the corresponding values for (100) silicon, all  $C_2$  values should be divided by 1.68.

Ambient	$B$	$B/A$
Dry O <sub>2</sub>	$C_1 = 7.72 \times 10^2 \mu\text{m}^2 \text{ hr}^{-1}$	$C_2 = 6.23 \times 10^6 \mu\text{m hr}^{-1}$
	$E_1 = 1.23 \text{ eV}$	$E_2 = 2.0 \text{ eV}$
Wet O <sub>2</sub>	$C_1 = 2.14 \times 10^2 \mu\text{m}^2 \text{ hr}^{-1}$	$C_2 = 8.95 \times 10^7 \mu\text{m hr}^{-1}$
	$E_1 = 0.71 \text{ eV}$	$E_2 = 2.05 \text{ eV}$
H <sub>2</sub> O	$C_1 = 3.86 \times 10^2 \mu\text{m}^2 \text{ hr}^{-1}$	$C_2 = 1.63 \times 10^8 \mu\text{m hr}^{-1}$
	$E_1 = 0.78 \text{ eV}$	$E_2 = 2.05 \text{ eV}$

• Above theory is great ... but usually, the equations are not used in practice, since measured data is available  
 ↳ Rather, oxidation growth charts are used

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### Factors Affecting Oxidation

- In summary, oxide thickness is dependent upon:
  1. Time of oxidation
  2. Temperature of oxidation
  3. Partial pressure of oxidizing species ( $\propto N_o$ )
- Also dependent on:
  4. Reactant type:
    - Dry  $\text{O}_2$
    - Water vapor  $\Rightarrow$  faster oxidation, since water has a higher solubility (i.e.,  $D$ ) in  $\text{SiO}_2$  than  $\text{O}_2$
  5. Crystal orientation:
    - <111>  $\leftarrow$  faster, because there are more bonds available at the Si-surface
    - <100>  $\leftarrow$  fewer interface traps; smaller # of unsatisfied Si-bonds at the Si- $\text{SiO}_2$  interface

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### Factors Affecting Oxidation

6. Impurity doping:
  - P: increases linear rate const.  
no affect on parabolic rate constant  
faster initial growth  $\rightarrow$  surface reaction rate limited
  - B: no effect on linear rate const.  
increases parabolic rate const.  
faster growth over an initial oxide  $\rightarrow$  diffusion faster

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## Thin Film Deposition

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## Thin Film Deposition

- Methods for film deposition:
  - ↳ Evaporation
  - ↳ Sputter deposition
  - ↳ Chemical vapor deposition (CVD)
  - ↳ Plasma enhanced chemical vapor deposition (PECVD)
  - ↳ Epitaxy
  - ↳ Electroplating
  - ↳ Atomic layer deposition (ALD)

**Evaporation:**

- Heat a metal (Al, Au) to the point of vaporization
- Evaporate to form a thin film covering the surface of the Si wafer
- Done under vacuum for better control of film composition

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## Evaporation

**Filament Evaporation System:**

1. Pump down to vacuum → reduces film contamination and allows better thickness control
2. Heat W filament → melt Al, wet filament
3. Raise temperature → evaporate Al

$$\text{mean free path} = \lambda = \frac{kT}{\sqrt{2\pi} Pd^2}$$

k = Boltzmann Constant  
 T = temperature  
 P = pressure  
 d = diameter of gas molecule

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## Evaporation (cont.)

- $\lambda$  can be ~60m for a 4Å particle at  $10^{-4}$  Pa ( $-0.75 \mu\text{Torr}$ )
  - ↳ thus, at  $0.75 \mu\text{Torr}$ , get straight line path from Al staple filament to wafer

**Problem:** Shadowing & Step Coverage

**Problem:** line of sight deposition

**Solns:**

- i. Rotate wafer during evaporation
- ii. Etch more gradual sidewalls

**Better Solution:** forget evaporation → sputter deposit the film!

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### Sputter Deposition

- Use an energetic plasma to dislodge atoms from a material target, allowing the atoms to settle on the wafer surface

Not as low a vacuum as evaporation (~100 Pa) (750 mTorr)

Vacuum Pump

Target (Al, SiO<sub>2</sub>, Si<sub>3</sub>N<sub>4</sub>, ZnO, Ti, ...)

plasma

Ar<sup>+</sup>

Ar<sup>+</sup>

wafer

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### Sputter Deposition Process

- Step-by-step procedure:**
  - Pump down to vacuum  
 $(\sim 100 \text{ Pa}) \rightarrow 1 \text{ Pa} = 9.8 \times 10^{-6} \text{ atm} \left( \frac{760 \text{ Torr}}{\text{atm}} \right) = 0.0075012 \text{ Torr}$   
7.5 mTorr
  - Flow gas (e.g., Ar)
  - Fire up plasma (create Ar<sup>+</sup> ions) → apply dc-bias (or RF for non-conductive targets)
  - Ar<sup>+</sup> ions bombard target (dislodge atoms)
  - Atoms make their way to the wafer in a more random fashion, since at this higher pressure,  $\lambda \sim 60 \mu\text{m}$  for a 4Å particle; plus, the target is much bigger
- Result:** better step coverage!

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### Problems With Sputtering

- Get some Ar in the film
- Substrate can heat up
  - ↪ up to ~350°C, causing nonuniformity across the wafer
  - ↪ but it still is more uniform than evaporation!
- Stress can be controlled by changing parameters (e.g., flow rate, plasma power) from pass to pass, but repeatability is an issue

conformal

nonuniform

conformal

uniform

- Solution:** use Chemical Vapor Deposition (CVD)

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### Chemical Vapor Deposition (CVD)

- Even better conformity than sputtering
- Form thin films on the surface of the substrate by thermal decomposition and/or reaction of gaseous compounds
  - ↪ Desired material is deposited directly from the gas phase onto the surface of the substrate
  - ↪ Can be performed at pressures for which  $\lambda$  (i.e., the mean free path) for gas molecules is small
  - ↪ This, combined with relatively high temperature leads to

**Excellent Conformal Step Coverage!**

- ↪ **Types of films:** polysilicon, SiO<sub>2</sub>, silicon nitride, SiGe, Tungsten (W), Molybdenum (M), Tantalum (Ta), Titanium (Ti), ...

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### The CVD Process

Reactant gas (+ inert diluting gases) are introduced into the reaction chamber

(a) Gas species move to the substrate

Gas Flow - Gas Stream

Reactants adsorb onto the substrate

(b) (c)(d)

Reaction by-products desorbed from surface

(e)

Atoms migrate and react chemically to form films

This determines the ultimate conformality of the film (i.e., determines step coverage)

Wafer

Energy required to drive reactions supplied by several methods: Thermal (i.e., heat), photons, electrons (i.e., plasma)

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### The CVD Process (cont.)

Step-by-Step CVD Sequence:

Gas phase processes

- Reactant gases (+ inert diluting gases) are introduced into reaction chamber
- Gas species move to the substrate
- Reactants adsorbed onto the substrate
- Atoms migrate and react chemically to form films. This determines to a large extent whether or not a film is conformal (i.e. better step coverage)
- Reaction by-products desorbed and removed from reaction chamber

Surface processes

Not Conformal  
low T  
not enough adatom migration

Conformal  
High T  
Plenty of adatom migration

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### CVD Modeling

Simplified Schematic:

$N_g$  = conc. of reactant molecules in the gas stream  
 $N_s$  = conc. of reactant molecules at the surface  
 $J_s$  = flux of gas molecules at the surface  
 $J_g$  = flux of molecules diffusing in from the gas stream

Governing Equations:

Effective diffusion const. for the gas molecule

$$J_s = k_s N_s \quad [k_s = \text{surface reaction rate const.}]$$

Vapor phase mass-transfer coefficient

$$J_g = \left( \frac{\bar{D}_g}{\delta} \right) (N_g - N_s) = h_g (N_g - N_s)$$

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### CVD Modeling (cont.)

Otherwise reactants will build up somewhere!

$$J = h_g \left( N_g - \frac{J}{k_s} \right) = h_g N_g - \frac{h_g J}{k_s}$$

$$J \left( 1 + \frac{h_g}{k_s} \right) = h_g N_g \rightarrow J = \frac{k_s h_g}{k_s + h_g} N_g = (k_s // h_g) N_g$$

growth rate =  $\frac{\text{flux}}{\# \text{ molecules incorporated/unit volume}} = \frac{J}{N}$

$$= \frac{J}{N} = \frac{k_s h_g}{k_s + h_g} \frac{N_g}{N} = (k_s // h_g) \frac{N_g}{N} = \text{growth rate}$$

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### CVD Modeling (cont.)

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- Case:  $k_s \gg h_g$   
 ↳ surface reaction rate  $\gg$  mass transfer rate

$$\text{growth rate} = h_g \frac{N_g}{N} \quad (\text{mass-transfer-limited})$$

- Case:  $h_g \gg k_s$   
 ↳ mass transfer rate  $\gg$  surface reaction rate

$$\text{growth rate} = k_s \frac{N_g}{N} \quad (\text{surface-reaction-limited})$$

~  $R_0^{-E_a/kT}$  (Arrhenius character)

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### Temperature Dependence of CVD

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The graph plots log(growth rate) on the y-axis against  $1/T$  (temperature) on the x-axis. A dashed line represents the mass transport limited regime, which is a straight line with a positive slope. A solid line represents the reaction rate limited regime, which follows the Arrhenius behavior (slope =  $-E_a$ ) at high  $1/T$  (low temperature) and transitions to a shallower slope at low  $1/T$  (high temperature).

Dep. Rate less dependent on T, here  
 ↳ for better control, better to operate here (@ higher T)

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### Atmospheric Pressure Reactor (APCVD)

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The schematic shows a cross-section of a reactor with a conveyor belt moving wafers through a chamber. Gas inlets for  $N_2$  and Gas are shown at the top. A heater is located below the wafers. Exhaust and a return line to the conveyor belt are shown at the bottom.

- Once used for silicon dioxide passivation in integrated circuits
- Substrates fed continuously
- Large diameter wafers
- Need high gas flow rates
- Mass transport-limited regime (high pressure, so tougher for gas to get to the wafer surface)

**Problems/Issues:**

- ↳ Wafers lay flat, and thus, incorporate foreign particles
- ↳ Poor step coverage

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### Low Pressure Reactor (LPCVD)

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- Many films available: polysilicon,  $SiGe$ ,  $Si_3N_4$ ,  $SiO_2$ , phosphosilicate glass (PSG), BPSG, W
- Temp.:  $300 \rightarrow 1150^\circ C$
- Press.:  $30 \rightarrow 250$  Pa ( $200mTorr \rightarrow 2Torr$ )
- Reaction rate limited; reduced pressure gives gas molecular high diffusivity; can supply reactants very fast!
- Can handle several hundred wafers at a time
- Excellent uniformity

The schematic shows a cross-section of a reactor with a quartz tube containing a three-zone furnace. Wafers are positioned in the tube. A pressure sensor is located at the top left, a gas inlet at the bottom left, and a pump at the right end. A load door is shown at the bottom left.

**Problems:**

- ↳ Low dep. rate (compared to atm.)
- ↳ Higher T (than atmospheric)
- ↳ In hot wall reactors, get deposition on tube walls (must clean)

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### Plasma-Enhanced CVD Reactor (PECVD)

- RF-induced glow discharge + thermal energy to drive reactions → allows lower temperature deposition with decent conformability
- Still low pressure

- Problems:**
  - Pin-holes
  - Non-stoichiometric films
  - Incorporation of H<sub>2</sub>, N<sub>2</sub>, O<sub>2</sub> contaminants in film; can lead to outgassing or bubbling in later steps

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### Polysilicon CVD

**Polysilicon Deposition:**

600°C → Fairly high temperature → conformal

$$\text{SiH}_4 \xrightarrow{600^\circ\text{C}} \text{Si} + 2\text{H}_2 \quad (\text{thermal decomposition of silane})$$

(conformal → high T)

LPCVD (25 to 150 Pa) → 100-200 Å/min

- In situ doping of polysilicon:**
  - n-type: add PH<sub>3</sub> (phosphine) or Arsine gases (but greatly reduces dep. rate)
  - p-type: add diborane gas (greatly increases dep. Rate)

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### Silicon Oxide CVD

**Silicon Dioxide Deposition:**

- After metallization (e.g., over aluminum)**
  - Temperature cannot exceed the Si-Al eutectic pt.: 577°C
  - Actually, need lower than this (<500°C) to prevent hillocks from growing on Al surfaces
  - Similar issues for copper (Cu) metallization
- Low temperature reactions:

LPCVD LTO Reactions	$\text{SiH}_4 + \text{O}_2 \xrightarrow{300-500^\circ\text{C}} \text{SiO}_2 + 2\text{H}_2$ <p>(silane)</p>	$4\text{PH}_3 + 5\text{O}_2 \xrightarrow{300-500^\circ\text{C}} 2\text{P}_2\text{O}_5 + 6\text{H}_2$ <p>(phosphine)</p>	$\text{SiO}_2 + 2\text{H}_2$	$2\text{P}_2\text{O}_5 + 6\text{H}_2$	<p>Phosphosilicate glass (PSG)</p>

- Above reactions: not very conformal step coverage → need higher T for this

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