


EE C245 - ME C218 Introduction to MEMS Design Fall 2012

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Lecture Module 3: Oxidation & Film Deposition

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Lecture Outline


- Reading: Senturia, Chpt. 3; Jaeger, Chpt. 2, 3, 6
 - ↳ Example MEMS fabrication processes
 - ↳ Oxidation
 - ↳ Film Deposition
 - Evaporation
 - Sputter deposition
 - Chemical vapor deposition (CVD)
 - Plasma enhanced chemical vapor deposition (PECVD)
 - Epitaxy
 - Atomic layer deposition (ALD)
 - Electroplating

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MEMS Fabrication

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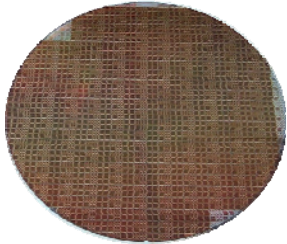


Making Mechanical Devices

- How best does one make a mechanical product?
- Assembly line production?
 - ✦ Pick and place parts
 - ✦ Used for many macroscopic mechanical products
 - ✦ Robotic automation greatly reduces cost
- **Problem:** difficult to do this with MEMS-scale parts (but not impossible, as we'll soon see ...)
- **Solution:** borrow from integrated circuit (IC) transistor technology
 - ✦ Use monolithic wafer-level fabrication methods
 - ✦ Harness IC's batch methods, where multiple devices are achieved all at once




Automobile Assembly Line

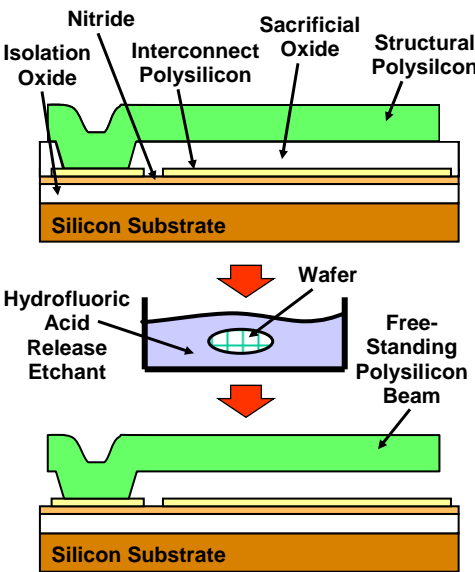


CMOS Integrated Circuit Wafer

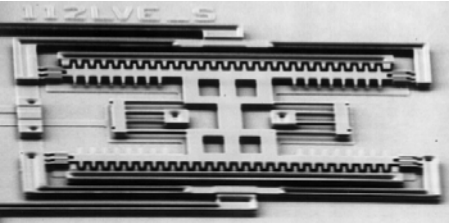
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Polysilicon Surface-Micromachining



- Uses IC fabrication instrumentation exclusively
- Variations: sacrificial layer thickness, fine- vs. large-grained polysilicon, *in situ* vs. POCL₃-doping



300 kHz Folded-Beam Micromechanical Resonator


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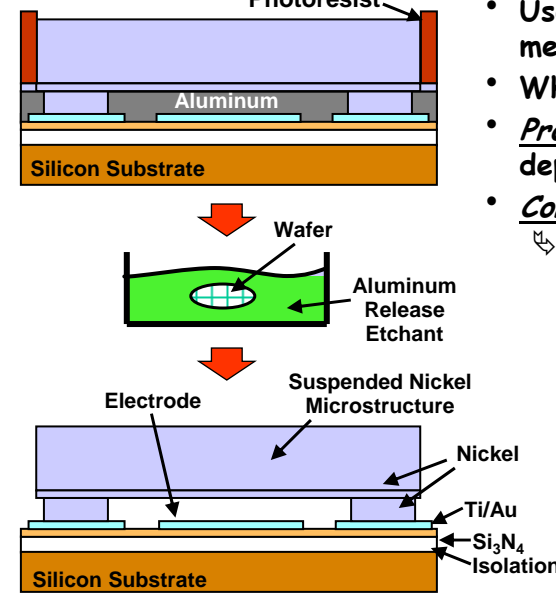
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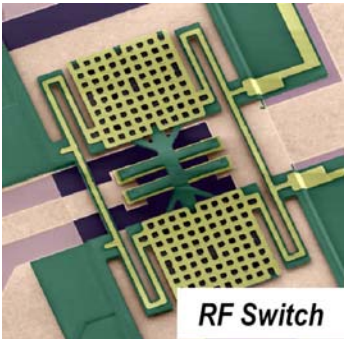
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Electroplating: Metal MEMS



- Use electroplating to obtain metal μ structures
- When thick: call it "LIGA"
- Pros: fast low temp deposition, very conductive
- Cons: drift, low mech. Q but may be solvable?




RF Switch

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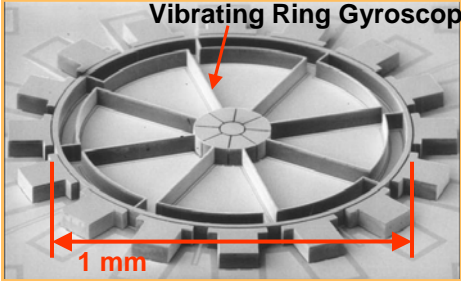
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Bulk Micromachining and Bonding

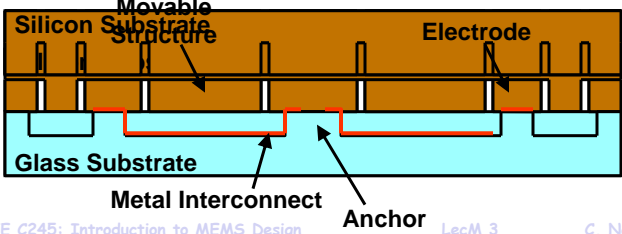
- Use the wafer itself as the structural material
- *Adv.* very large aspect ratios, thick structures
- *Example:* deep etching and wafer bonding



Micromechanical Vibrating Ring Gyroscope

1 mm

[Najafi, Michigan]



Movable Substrate Structure

Silicon Substrate


Electrode

Glass Substrate

Metal Interconnect

Anchor

[Pisano, UC Berkeley]



Microrotor (for a microengine)

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Oxidation


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Thermal Oxidation of Silicon

- Achieved by heating the silicon wafer to a high temperature (~900°C to 1200°C) in an atmosphere containing pure oxygen or water vapor
- Enabling reactions:

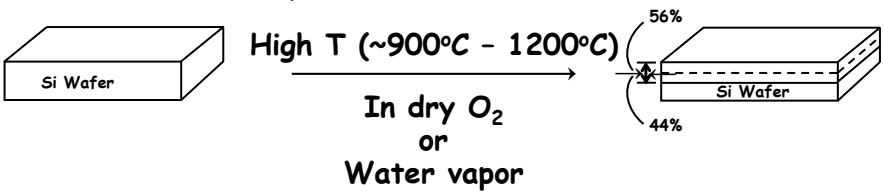
For dry oxygen:

$$\text{Si} + \text{O}_2 \rightarrow \text{SiO}_2$$


For water vapor:

$$\text{Si} + 2\text{H}_2\text{O} \rightarrow \text{SiO}_2 + 2\text{H}_2$$

Schematically:



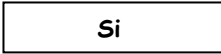
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Oxidation Modeling

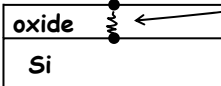
- Initially: (no oxide @ surface)

gas stream



⇒ Growth rate determined by reaction rate @ the surface
- As oxide builds up:

gas stream



Reactant must diffuse to Si surface where the oxidation reaction takes place

⇒ Growth rate governed more by rate of diffusion to the silicon-oxide interface

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Oxidation Modeling (cont.)

reactant concentration

N_0 N_i

SiO_2 Si

J

X_{ox}

surface Si-SiO_2 interface distance from surface

N_o = reactant conc. at oxide surface [in cm^{-2}]

N_i = reactant conc. at Si-SiO_2 interface

J = reactant flux = $-D \frac{\partial N(x,t)}{\partial x}$ [Fick's 1st Law of Diffusion]

Diffusion coeff. [in $\mu\text{m/hr}$ or m/s]

In the SiO_2 :

$$J = D \frac{(N_o - N_i)}{X_{ox}} = \text{constant} \quad (1)$$

[in # particles/($\text{cm}^2 \cdot \text{s}$)]

Assumption that the reactant does not accumulate in the oxide.

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Oxidation Modeling (cont.)

At the Si-SiO_2 interface:

Oxidation rate $\propto N_i \therefore J \propto N_i \Rightarrow J = k_s N_i \quad (2)$

Reaction rate constant @ Si-SiO_2 interface


Combining (1) and (2):

$$\left[N_i = \frac{J}{k_s} \right] \Rightarrow J = D \left(\frac{N_o - J/k_s}{X_{ox}} \right)$$

$$JX_{ox} = DN_o - \frac{DJ}{k_s} \rightarrow J \left(X_{ox} + \frac{D}{k_s} \right) = DN_o$$

$$\therefore J = \frac{DN_o}{X_{ox} + \frac{D}{k_s}} = \text{Flux of reactants}$$

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 **Oxidation Modeling (cont.)**

Find an expression for $X_{OX}(t)$:


Rate of change of oxide layer thickness w/time $\left. \vphantom{\frac{dX_{OX}}{dt}} \right\} = \frac{dX_{OX}}{dt} = \frac{J}{M} = \frac{DN_o/M}{X_{OX} + D/k_s}$ (3) oxidizing flux \swarrow

$\left. \vphantom{\frac{dX_{OX}}{dt}} \right\} \begin{aligned} \text{\# of molecules of oxidizing} \\ \text{species incorporated into a} \\ \text{unit volume of oxide} \end{aligned} = \begin{aligned} &2.2 \times 10^{22} \text{ cm}^{-3} \text{ for } O_2 \\ &4.4 \times 10^{22} \text{ cm}^{-3} \text{ for } H_2O \end{aligned}$

Solve (3) for $X_{OX}(t)$: [Initial condition $X_{OX}(t=0) = X_i$]

$$\frac{dX_{OX}}{dt} = \frac{DN_o/M}{X_{OX} + D/k_s} \quad \Rightarrow \quad \int_{X_i}^{X_{OX}} \left(X_{OX} + \frac{D}{k_s} \right) dX_{OX} = \int_0^t \frac{DN_o}{M} dt$$

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 **Oxide Thickness Versus Time**

Result:

$X_{OX}(t) = \frac{A}{2} \left\{ \left[1 + \frac{4B}{A^2} (t + \tau) \right]^{1/2} - 1 \right\}$


$\left. \vphantom{\frac{4B}{A^2}} \right\} \begin{aligned} &\text{additional time required} \\ &\text{(to go from } X_i \rightarrow X_{OX}) \end{aligned}$ $\left. \vphantom{\frac{4B}{A^2}} \right\} \begin{aligned} &\text{time required to grow } X_i \\ &[X_i = \text{initial oxide thickness}] \end{aligned}$

where $A = \frac{2D}{k_s}$ $\tau = \frac{X_i^2}{B} + \frac{X_i}{(B/A)}$

$B = \frac{2DN_o}{M}$ $D = D_o \exp\left(-\frac{E_A}{kT}\right)$

$\left[\begin{aligned} &\text{i.e., D governed by an Arrhenius} \\ &\text{relationship} \rightarrow \text{temperature dependent} \end{aligned} \right]$

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Oxidation Modeling (cont.)

For shorter times:

$$\left[(t + \tau) \ll \frac{A^2}{4B} \right] \Rightarrow X_{ox}(t) = \underbrace{\left(\frac{B}{A} \right)}_{\text{linear growth rate constant}} (t + \tau) \Rightarrow \text{oxide growth limited by reaction at the Si-SiO}_2 \text{ interface}$$

Taylor expansion (first term after 1's cancel)

For long oxidation times: oxide growth diffusion-limited

$$\left[(t + \tau) \gg \frac{A^2}{4B} \right] \Rightarrow X_{ox}(t) = \sqrt{B(t + \tau)} \approx \sqrt{Bt}$$

$t \gg \tau$ Parabolic rate constant


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Oxidation Rate Constants

Table 6-2 Rate constants describing (111) silicon oxidation kinetics at 1 Atm total pressure. For the corresponding values for (100) silicon, all C_2 values should be divided by 1.68.

Ambient	B	B/A
Dry O ₂	$C_1 = 7.72 \times 10^2 \mu\text{m}^2 \text{hr}^{-1}$ $E_1 = 1.23 \text{ eV}$	$C_2 = 6.23 \times 10^6 \mu\text{m hr}^{-1}$ $E_2 = 2.0 \text{ eV}$
Wet O ₂	$C_1 = 2.14 \times 10^2 \mu\text{m}^2 \text{hr}^{-1}$ $E_1 = 0.71 \text{ eV}$	$C_2 = 8.95 \times 10^7 \mu\text{m hr}^{-1}$ $E_2 = 2.05 \text{ eV}$
H ₂ O	$C_1 = 3.86 \times 10^2 \mu\text{m}^2 \text{hr}^{-1}$ $E_1 = 0.78 \text{ eV}$	$C_2 = 1.63 \times 10^8 \mu\text{m hr}^{-1}$ $E_2 = 2.05 \text{ eV}$

- Above theory is great ... but usually, the equations are not used in practice, since measured data is available
 - Rather, oxidation growth charts are used

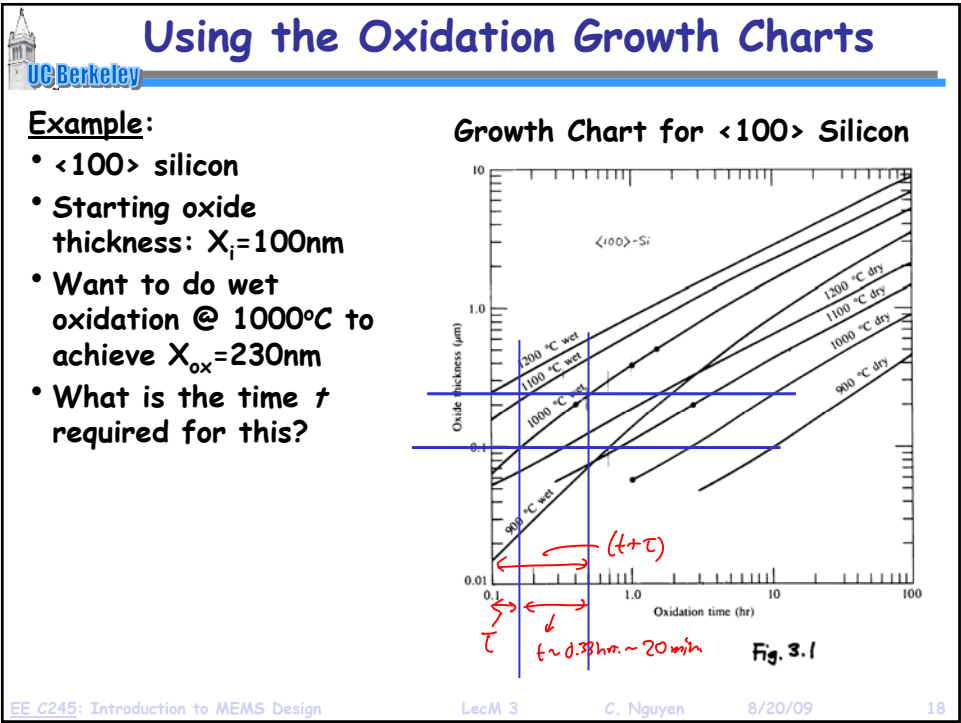
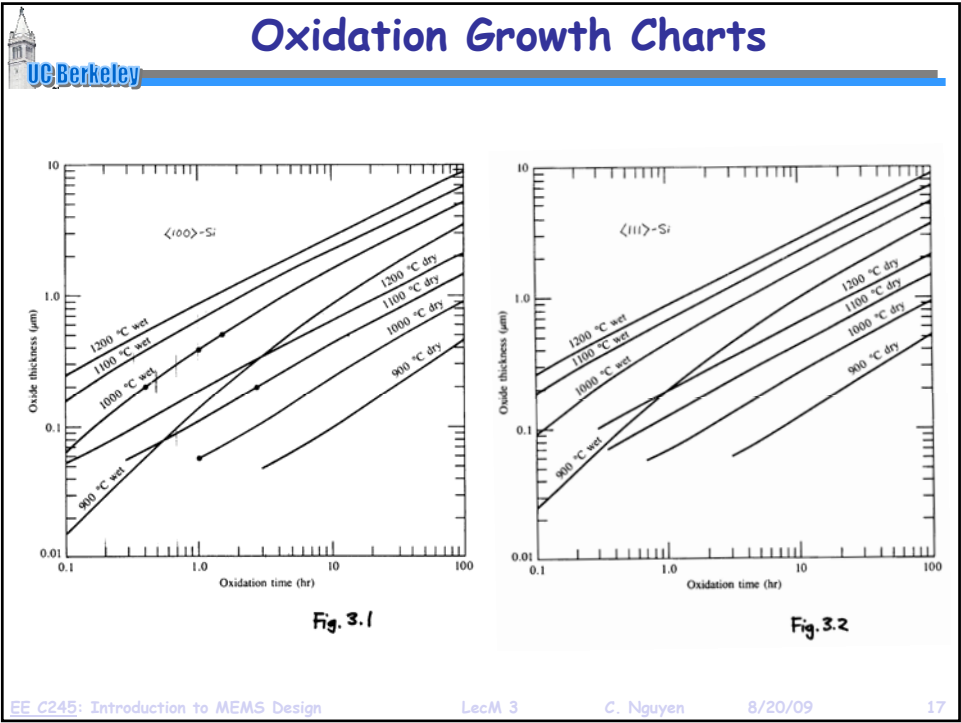
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Factors Affecting Oxidation

- In summary, oxide thickness is dependent upon:
 1. Time of oxidation
 2. Temperature of oxidation
 3. Partial pressure of oxidizing species ($\propto N_O$)
- Also dependent on:
 4. Reactant type:
 - Dry O_2
 - Water vapor \Rightarrow faster oxidation, since water has a higher solubility (i.e., D) in SiO_2 than O_2
 5. Crystal orientation:
 - $\langle 111 \rangle \leftarrow$ faster, because there are more bonds available at the Si-surface
 - $\langle 100 \rangle \leftarrow$ fewer interface traps; smaller # of unsatisfied Si-bonds at the Si- SiO_2 interface


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Factors Affecting Oxidation

6. Impurity doping:
 - P: increases linear rate const.
 - no affect on parabolic rate constant
 - faster initial growth \rightarrow surface reaction rate limited
 - B: no effect on linear rate const.
 - increases parabolic rate const.
 - faster growth over an initial oxide \rightarrow diffusion faster

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Thin Film Deposition

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Thin Film Deposition

- **Methods for film deposition:**
 - ↗ Evaporation
 - ↗ Sputter deposition
 - ↗ Chemical vapor deposition (CVD)
 - ↗ Plasma enhanced chemical vapor deposition (PECVD)
 - ↗ Epitaxy
 - ↗ Electroplating
 - ↗ Atomic layer deposition (ALD)

Evaporation:

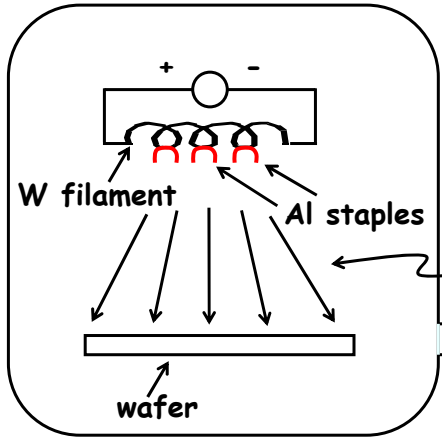
- Heat a metal (Al, Au) to the point of vaporization
- Evaporate to form a thin film covering the surface of the Si wafer
- Done under vacuum for better control of film composition

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Evaporation

Filament Evaporation System:



1. Pump down to vacuum
→ reduces film contamination and allows better thickness control
2. Heat W filament → melt Al, wet filament
3. Raise temperature → evaporate Al


mean free path = $\lambda = \frac{kT}{\sqrt{2\pi} Pd^2}$

Vacuum Pump

W filament
Al staples
wafer

k = Boltzmann Constant
T = temperature
P = pressure
d = diameter of gas molecule

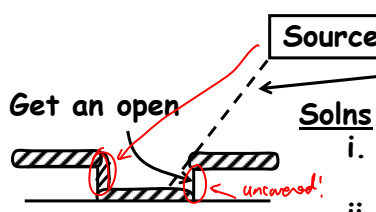
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Evaporation (cont.)

- λ can be ~60m for a 4Å particle at 10^{-4} Pa (~0.75 μTorr)
 ↳ thus, at 0.75 μTorr, get straight line path from Al staple filament to wafer

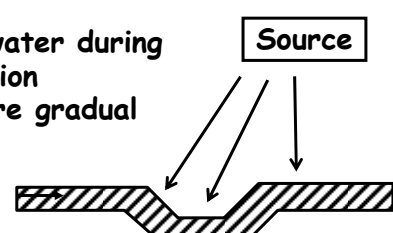
Problem: Shadowing & Step Coverage



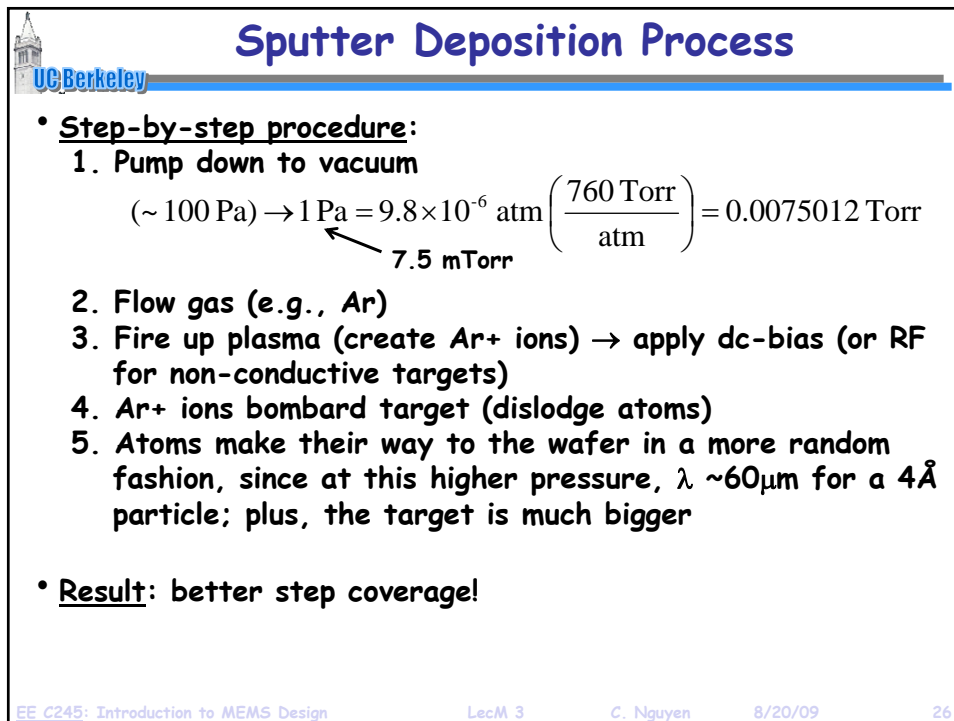
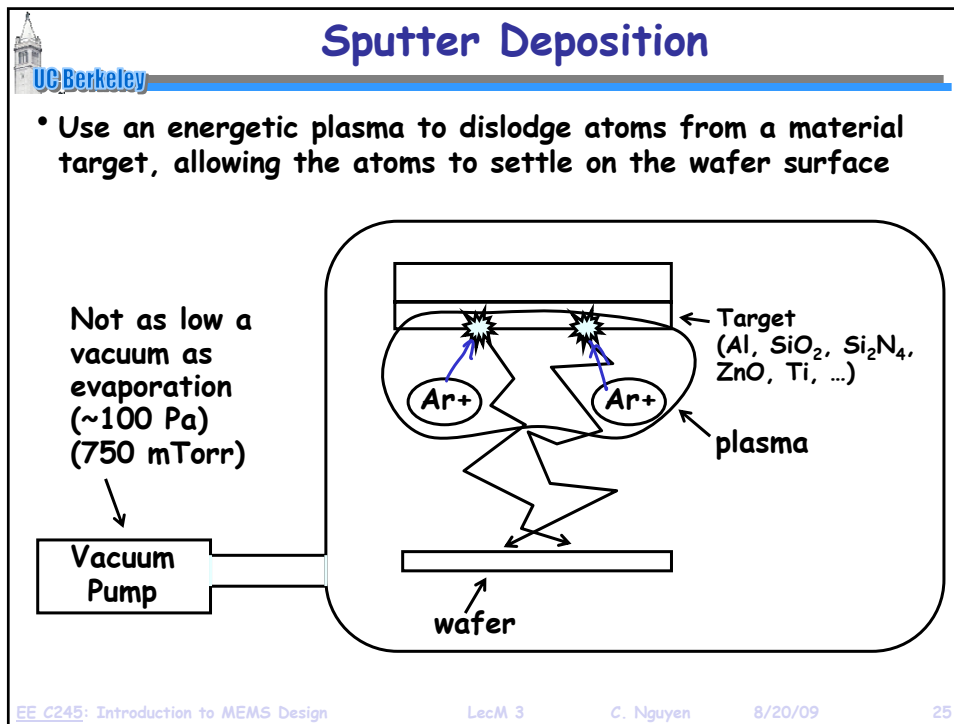
Solns:


- i. Rotate wafer during evaporation
- ii. Etch more gradual sidewalls

Better Solution: forget evaporation → sputter deposit the film!



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Problems With Sputtering

1. Get some Ar in the film
2. Substrate can heat up
 - ↳ up to $\sim 350^{\circ}\text{C}$, causing nonuniformity across the wafer
 - ↳ but it still is more uniform than evaporation!
3. Stress can be controlled by changing parameters (e.g., flow rate, plasma power) from pass to pass, but repeatability is an issue

• Solution: use Chemical Vapor Deposition (CVD)


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Chemical Vapor Deposition (CVD)

- Even better conformity than sputtering
- Form thin films on the surface of the substrate by thermal decomposition and/or reaction of gaseous compounds
 - ↳ Desired material is deposited directly from the gas phase onto the surface of the substrate
 - ↳ Can be performed at pressures for which λ (i.e., the mean free path) for gas molecules is small
 - ↳ This, combined with relatively high temperature leads to



Excellent Conformal Step Coverage!

- ↳ Types of films: polysilicon, SiO_2 , silicon nitride, SiGe , Tungsten (W), Molybdenum (M), Tantalum (Ta), Titanium (Ti), ...


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The CVD Process

Reactant gas (+ inert diluting gases) are introduced into the reaction chamber

(a) Gas species move to the substrate

Gas Flow - Gas Stream

(b) Reactants adsorb onto the substrate

(c) Atoms migrate and react chemically to form films

(d) This determines the ultimate conformality of the film (i.e., determines step coverage)

(e) Reaction by-products desorbed from surface

Wafer

Energy required to drive reactions supplied by several methods: Thermal (i.e., heat), photons, electrons (i.e., plasma)


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The CVD Process (cont.)

Step-by-Step CVD Sequence:

Gas phase processes

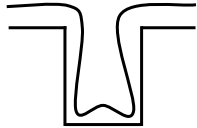
Surface processes

a) Reactant gases (+ inert diluting gases) are introduced into reaction chamber

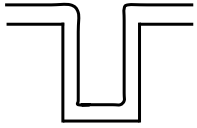
b) Gas species move to the substrate

c) Reactants adsorbed onto the substrate

d) Atoms migrate and react chemically to form films
This determines to a large extent whether or not a film is conformal (i.e. better step coverage)



Not Conformal
low T
not enough adatom migration



Conformal
High T
Plenty of adatom migration

e) Reaction by-products desorbed and removed from reaction chamber

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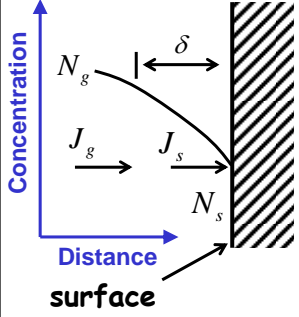
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CVD Modeling

Simplified Schematic:



N_g = conc. of reactant molecules in the gas stream

N_s = conc. of reactant molecules at the surface

J_s = flux of gas molecules at the surface

J_g = flux of molecules diffusing in from the gas stream

Governing Equations:


Effective diffusion const. for the gas molecule

$$J_s = k_s N_s \quad [k_s = \text{surface reaction rate const.}]$$

Vapor phase mass-transfer coefficient

$$J_g = \left(\frac{\bar{D}_g}{\delta} \right) (N_g - N_s) = h_g (N_g - N_s)$$

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CVD Modeling (cont.)

Otherwise reactants will build up somewhere!

$J_s = J_g = J$, $N_s = \frac{J}{k_s}$


$$J = h_g \left(N_g - \frac{J}{k_s} \right) = h_g N_g - \frac{h_g J}{k_s}$$

$$J \left(1 + \frac{h_g}{k_s} \right) = h_g N_g \rightarrow J = \frac{k_s h_g}{k_s + h_g} N_g = (k_s \parallel h_g) N_g$$

growth rate = $\frac{\text{flux}}{\text{\# molecules incorporated/unit volume}} = \frac{J}{N}$

$$= \frac{J}{N} = \frac{k_s h_g}{k_s + h_g} \frac{N_g}{N} = (k_s \parallel h_g) \frac{N_g}{N} = \text{growth rate}$$

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CVD Modeling (cont.)

- Case: $k_s \gg h_g$
 \Rightarrow surface reaction rate \gg mass transfer rate

$\text{growth rate} = h_g \frac{N_g}{N}$

(mass-transfer-limited)

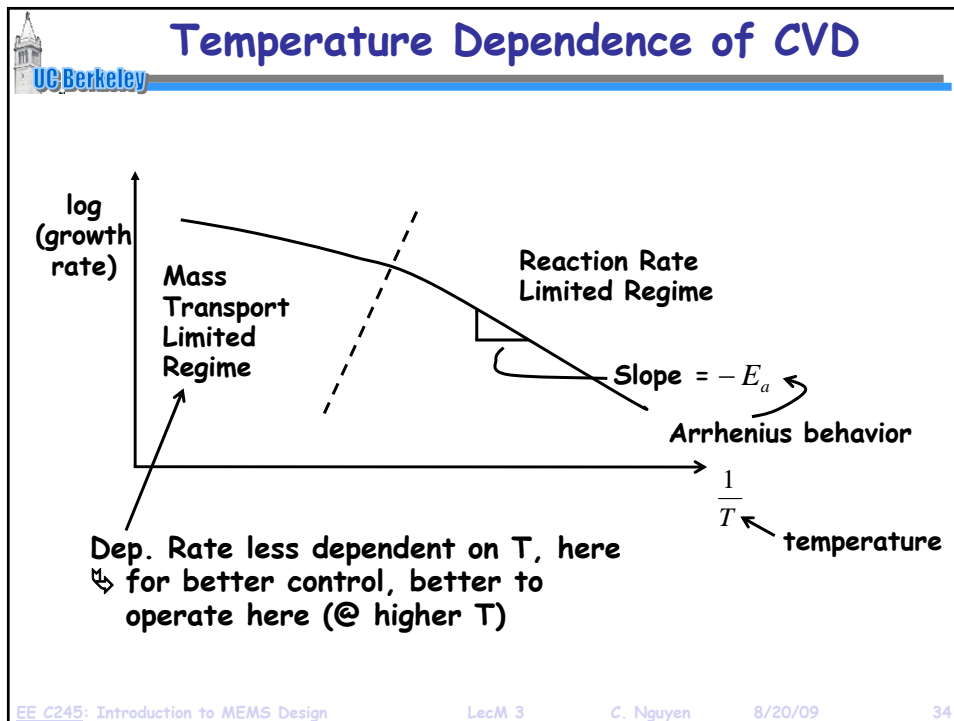
- Case: $h_g \gg k_s$
 \Rightarrow mass transfer rate \gg surface reaction rate


$\text{growth rate} = k_s \frac{N_g}{N}$

(surface-reaction-limited)

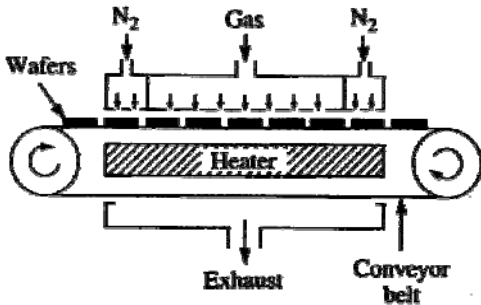
$\sim R_o^{-E_a/kT}$ (Arrhenius character)

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Atmospheric Pressure Reactor (APCVD)




- Once used for silicon dioxide passivation in integrated circuits
- Substrates fed continuously
- Large diameter wafers
- Need high gas flow rates
- Mass transport-limited regime (high pressure, so tougher for gas to get to the wafer surface)

• **Problems/Issues:**

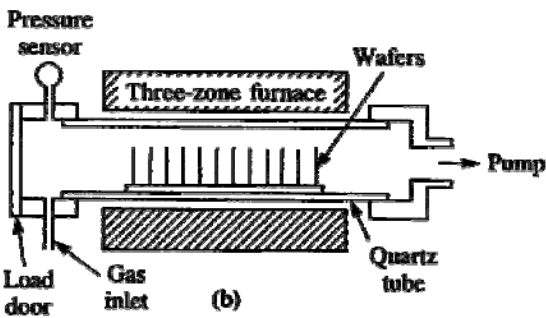
- ↳ Wafers lay flat, and thus, incorporate foreign particles
- ↳ Poor step coverage

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Low Pressure Reactor (LPCVD)


- Many films available: polysilicon, SiGe, Si₃N₄, SiO₂, phosphosilicate glass (PSG), BPSG, W
- Temp.: 300 → 1150°C
- Press.: 30 → 250 Pa (200mTorr → 2Torr)
- Reaction rate limited; reduced pressure gives gas molecular high diffusivity; can supply reactants very fast!
- Can handle several hundred wafers at a time
- Excellent uniformity



• **Problems:**


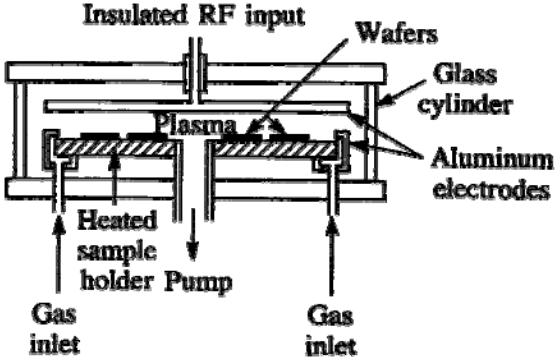
- ↳ Low dep. rate (compared to atm.)
- ↳ Higher T (than atmospheric)
- ↳ In hot wall reactors, get deposition on tube walls (must clean)

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Plasma-Enhanced CVD Reactor (PECVD)

- RF-induced glow discharge + thermal energy to drive reactions → allows lower temperature deposition with decent conformability
- Still low pressure

- Problems:
 - ↳ Pin-holes
 - ↳ Non-stoichiometric films
 - ↳ Incorporation of H₂, N₂, O₂ contaminants in film; can lead to outgassing or bubbling in later steps

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Polysilicon CVD

Polysilicon Deposition:

$\text{SiH}_4 \xrightarrow{600^\circ\text{C}} \text{Si} + 2\text{H}_2$ (thermal decomposition of silane)


(conformal → high T)

LPCVD (25 to 150 Pa) → 100-200 Å/min

→ Fairly high temperature → conformal

- In situ doping of polysilicon:
 - ↳ n-type: add PH₃ (phosphine) or Arsine gases (but greatly reduces dep. rate)
 - ↳ p-type: add diborane gas (greatly increases dep. Rate)

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Silicon Oxide CVD

Silicon Dioxide Deposition:

- After metallization (e.g., over aluminum)
 - ↳ Temperature cannot exceed the Si-Al eutectic pt.: 577°C
 - ↳ Actually, need lower than this (<500°C) to prevent hillocks from growing on Al surfaces
 - ↳ Similar issues for copper (Cu) metallization
- Low temperature reactions:

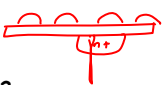
LPCVD
LTO
Reactions

{


$$\begin{array}{l} \text{SiH}_4 + \text{O}_2 \xrightarrow{300-500^\circ\text{C}} \text{SiO}_2 + 2\text{H}_2 \\ \text{(silane)} \\ \\ 4\text{PH}_3 + 5\text{O}_2 \xrightarrow{300-500^\circ\text{C}} 2\text{P}_2\text{O}_5 + 6\text{H}_2 \\ \text{(phosphine)} \end{array}$$

Phosphosilicate glass (PSG)

• Above reactions: not very conformal step coverage → need higher T for this



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Silicon Oxide CVD (cont.)

- Phosphosilicate glass can be reflow
 - ↳ 6-8 wt. % allows reflow @ 1000-1100°C
 - ↳ Very useful to achieve smoother topography
 - ↳ Lower concentration → won't reflow
 - ↳ Higher concentration → corrodes Al if moisture is present
 - ↳ 5-15% P can be used as a diffusion source to dope Si
- Before metallization:
 - ↳ Can use higher temperature → better uniformity and step coverage

HTO {

$$\text{SiCl}_2\text{H}_2 + 2\text{N}_2\text{O} \xrightarrow{\sim 900^\circ\text{C}} \text{SiO}_2 + 2\text{N}_2 + 2\text{HCl}$$

(dichlorosilane) (Nitrous oxide) (nice conformal step coverage)

or ...

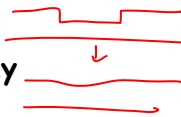
Handwritten notes:

↑↑↑ PTC P P P P


↓ ↓ ↓ p-doped Si

↑↑↑ PSG P P P P

diffuse @ high T



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Silicon Oxide CVD (cont.)

$\text{Si}(\text{OC}_2\text{H}_5)_4$
(Tetraethylorthosilicate)
(TEOS)

$\xrightarrow{650-750^\circ\text{C}}$

$\text{SiO}_2 + \text{by-products}$
(excellent uniformity &
conformal step coverage)

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